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**COMMERCIAL-SCALE DEMONSTRATION OF THE
LIQUID PHASE METHANOL (LPMEOH™) PROCESS**

ENVIRONMENTAL MONITORING REPORT NO. 1

For The Period

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ACRONYMS AND DEFINITIONS

| | | |
|------------------------|---|---|
| Acurex | - | Acurex Environmental Corporation |
| Air Products | - | Air Products and Chemicals, Inc. |
| AFDU | - | Alternative Fuels Development Unit - The "LaPorte PDU" |
| Balanced Gas | - | A syngas with a composition of hydrogen (H ₂), carbon monoxide (CO), and carbon dioxide (CO ₂) in stoichiometric balance for the production of methanol |
| BOD | - | Biochemical Oxygen Demand |
| Carbon Monoxide Gas | - | A syngas containing primarily carbon monoxide (CO); also called CO Gas |
| Crude Grade Methanol | - | Underflow from rectifier column (29C-20), defined as 80 wt% minimum purity; requires further distillation in existing Eastman equipment prior to use |
| DME | - | dimethyl ether |
| DOE | - | United States Department of Energy |
| DOE-FETC | - | The DOE's Federal Energy Technology Center (Project Team) |
| DOE-HQ | - | The DOE's Headquarters - Coal Fuels and Industrial Systems (Project Team) |
| DTP | - | Demonstration Test Plan - The four-year Operating Plan for Phase 3, Task 2 Operation |
| DVT | - | Design Verification Testing |
| Eastman | - | Eastman Chemical Company |
| EIV | - | Environmental Information Volume |
| EMP | - | Environmental Monitoring Plan |
| EMR | - | Environmental Monitoring Report |
| EPRI | - | Electric Power Research Institute |
| HAPs | - | Hazardous Air Pollutants |
| Hydrogen Gas | - | A syngas containing an excess of hydrogen (H ₂) over the stoichiometric balance for the production of methanol; also called H ₂ Gas |
| IGCC | - | Integrated Gasification Combined Cycle, a type of electric power generation plant |
| IGCC/OTM | - | An IGCC plant with a "Once-Thru Methanol" plant (the LPMEOH™ Process) added-on |
| KSCF | - | Thousand Standard Cubic Feet |
| KSCFH | - | Thousand Standard Cubic Feet per Hour |
| LaPorte PDU | - | The DOE-owned experimental unit (PDU) located adjacent to Air Products' industrial gas facility at LaPorte, Texas, where the LPMEOH™ process was successfully piloted |
| LDAR | - | Leak Detection and Repair |
| LPDME | - | Liquid Phase DME process, for the production of DME as a mixed coproduct with methanol |
| LPMEOH™ | - | Liquid Phase Methanol (the technology to be demonstrated) |
| Main Plant Purge | - | Unreacted synthesis gas stream from LPMEOH™ process returned to Eastman's fuel gas header |
| mg/m ³ | - | Milligrams per cubic meter |
| NEPA | - | National Environmental Policy Act |
| NPDES | - | National Pollutant Discharge Elimination System |
| OSHA | - | Occupational Safety and Health Administration |
| Partnership | - | Air Products Liquid Phase Conversion Company, L.P. |
| PDU | - | Process Development Unit |
| PFD | - | Process Flow Diagram(s) |
| ppbv | - | parts per billion (volume basis) |
| Project | - | Production of Methanol/DME Using the LPMEOH™ Process at an Integrated Coal Gasification Facility |
| psia | - | Pounds per Square Inch (Absolute) |
| psig | - | Pounds per Square Inch (gauge) |
| P&ID | - | Piping and Instrumentation Diagram(s) |
| RCRA | - | Resource and Conservation Recovery Act |
| Refined Grade Methanol | - | Distilled methanol, defined as 99.8wt% minimum purity; used directly in downstream Eastman processes |
| SCFH | - | Standard Cubic Feet per Hour |
| SL/hr-kg | - | Standard Liter(s) per Hour per Kilogram of Catalyst |

ACRONYMS AND DEFINITIONS (cont'd)

| | | |
|---------------|---|--|
| Syngas | - | Abbreviation for Synthesis Gas |
| Synthesis Gas | - | A gas containing primarily hydrogen (H ₂) and carbon monoxide (CO), or mixtures of H ₂ and CO; intended for "synthesis" in a reactor to form methanol and/or other hydrocarbons (synthesis gas may also contain CO ₂ , water, and other gases) |
| Tie-in(s) | - | the interconnection(s) between the LPMEOH™ Process Demonstration Facility and the Eastman Facility |
| TLV | - | Threshold Limit Value |
| TPD | - | Ton(s) per Day |
| WBS | - | Work Breakdown Structure |
| wt | - | Weight |

1. Introduction

The Liquid Phase Methanol (LPMEOH™) demonstration project at Kingsport, Tennessee, is a \$213.7 million cooperative agreement between the U.S. Department of Energy (DOE) and Air Products Liquid Phase Conversion Company, L. P. (the Partnership). Air Products and Chemicals, Inc. (Air Products) and Eastman Chemical Company (Eastman) formed the Partnership to execute the Demonstration Project. A demonstration unit producing 80,000 gallons per day (260 TPD) of methanol was designed, constructed, and has begun operation at a site located at the Eastman complex in Kingsport. The Partnership will own and operate the facility for the four-year demonstration period.

This project is sponsored under the DOE's Clean Coal Technology Program, and its primary objective is to "demonstrate the production of methanol using the LPMEOH™ Process in conjunction with an integrated coal gasification facility." The project will also demonstrate the suitability of the methanol produced for use as a chemical feedstock or as a low-sulfur dioxide, low-nitrogen oxides alternative fuel in stationary and transportation applications. The project may also demonstrate the production of dimethyl ether (DME) as a mixed coproduct with methanol, if laboratory- and pilot-scale research and market verification studies show promising results. If implemented, the DME would be produced during the last six months of the four-year demonstration period.

The LPMEOH™ process is the product of a cooperative development effort by Air Products and the DOE in a program that started in 1981. It was successfully piloted at a 10-TPD rate in the DOE-owned experimental unit at Air Products' LaPorte, Texas, site. This demonstration project is the culmination of that extensive cooperative development effort.

2. Project Description

The demonstration unit, which occupies an area of 0.6 acre, is integrated into the existing 4,000-acre Eastman complex located in Kingsport, Tennessee. The Eastman complex employs approximately 12,000 people. In 1983, Eastman constructed a coal gasification facility utilizing Texaco technology. The syngas generated by this gasification facility is used to produce carbon monoxide and methanol. Both of these products are used to produce methyl acetate and ultimately cellulose acetate and acetic acid. The availability of this highly reliable coal gasification facility was the major factor in selecting this location for the LPMEOH™ Process Demonstration. Three different feed gas streams (hydrogen gas, carbon monoxide gas, and balanced gas) will be diverted from existing operations to the LPMEOH™ Demonstration Unit, thus providing the range of coal-derived synthesis gas (syngas) ratios (hydrogen to carbon monoxide) needed to meet the technical objectives of the demonstration project.

For descriptive purposes and for design and construction scheduling, the project has been divided into four major process areas with their associated equipment:

- *Reaction Area* - Syngas preparation and methanol synthesis reaction equipment.
- *Purification Area* - Product separation and purification equipment.
- *Catalyst Preparation Area* - Catalyst and slurry preparation and disposal equipment.
- *Storage/Utility Area* - Methanol product, slurry, and oil storage equipment.

The physical appearance of this facility closely resembles the adjacent Eastman process plants, including process equipment in steel structures.

- *Reaction Area*

The reaction area includes feed gas compressors, catalyst guard beds, the reactor, a steam drum, separators, heat exchangers, and pumps. The equipment is supported by a matrix of structural steel. The most salient feature is the reactor, since with supports, it is approximately 84-feet tall.

- *Purification Area*

The purification area features two distillation columns with supports; one is approximately 82-feet tall, and the other 97-feet tall. These vessels resemble the columns of the surrounding process areas. In addition to the columns, this area includes the associated reboilers, condensers, air coolers, separators, and pumps.

- *Catalyst Preparation Area*

The catalyst preparation area consists of a building with a roof and partial walls, in which the catalyst preparation vessels, slurry handling equipment, and spent slurry disposal equipment are housed. In addition, a hot oil utility system is included in the area.

- *Storage/Utility Area*

The storage/utility area includes two diked lot-tanks for methanol, two tanks for oil storage, a slurry holdup tank, a trailer loading/unloading area, and an underground oil/water separator. A vent stack for safety relief devices is located in this area.

3. Process Description

The LPMEOH™ Demonstration Unit is integrated with Eastman's coal gasification facility. A simplified process flow diagram is included in Appendix A. Syngas is introduced into the slurry reactor, which contains a slurry of liquid mineral oil with suspended solid particles of catalyst. The syngas dissolves through the mineral oil, contacts the catalyst, and reacts to form methanol. The heat of reaction is absorbed by the slurry and is removed from the slurry by steam coils. The methanol vapor leaves the reactor, is condensed to a liquid, sent to the distillation columns for removal of higher alcohols, water, and other impurities, and is then stored in the day tanks for sampling before being sent to Eastman's methanol storage. Most of the unreacted syngas is recycled back to the reactor with the syngas recycle compressor, improving cycle efficiency. The methanol will be used for downstream

feedstocks and in off-site fuel testing to determine its suitability as a transportation fuel and as a fuel for stationary applications in the power industry.

Demonstration Test Plan

After the start-up of the LPMEOH™ Demonstration Unit, a four-year test plan is being performed by Air Products and Eastman. The goals of the Test Plan are structured to meet the commercialization objectives for the LPMEOH™ Process. Excerpts from Commercialization Objectives from the program Statement of Work are included here to provide the global perspective of the Demonstration Plan:

"Primary Objective

The primary objective of the Project is to demonstrate the commercial scale production of methanol using the LPMEOH™ Process...

The LPMEOH™ Process technology is expected to be commercialized as part of an IGCC electric power generation system. Therefore, the Project incorporates the commercially important aspects of the operation of the LPMEOH™ Process which would enhance IGCC power generation. These important aspects of LPMEOH™ Process integrations are:

- The coproduction of electric power and of high value liquid transportation fuels and/or chemical feedstocks from coal. This coproduction requires that the partial conversion of synthesis gas to storable liquid products be demonstrated.
- Using an energy load following operating concept which allows conversion of off-peak energy, at attendant low value, into peak energy commanding a higher value. The load-following concept makes use of gasifier capacity that is under utilized during low-demand periods by using the LPMEOH™ Process to convert the excess synthesis gas to a storable liquid fuel for use in electric power generation during the peak energy periods. This operating concept requires that on/off and synthesis gas load following capabilities be demonstrated...

During operation, the instrumentation system will allow for the collection of engineering data, analysis and reporting which will be done by on-site technical personnel. Typical reporting will include on-stream factors, material and energy balances, reactor and equipment performance, comparison with laboratory and LaPorte Alternative Fuels Development Unit (AFDU) results, conversion efficiencies and catalyst activity...

Secondary Objective

A secondary objective of the Project is to demonstrate the production of DME (Dimethyl ether) as a mixed coproduct with methanol...

Subject to Design Verification Testing (DVT), the Partnership proposes to enhance the Project by including the demonstration of the slurry reactor's capability to produce DME as a mixed co-product with methanol...

DVT is required to address issues such as catalyst activity and stability and to provide data for engineering design and demonstration decision making...

At the conclusion of the DVT Steps, a joint Partnership/DOE decision will be made regarding continuation of the methanol/DME demonstration. Timing of the final decision must ensure that the necessary design, procurement, construction and commissioning can be completed to allow for (Phase 3, Task 2.2) operation at the end of the primary LPMEOH™ process demonstration period."

The full Demonstration Test Plan (issued September 1996) provides details in the strategy and conditions to be tested during the four-year operating period.

4. Environmental Monitoring Plan (EMP) Description

Air Products Liquid Phase Conversion Company, L.P., has constructed and is operating the 260 ton-per-day Liquid Phase Methanol (LPMEOH™) Demonstration Unit at the Eastman Chemical facility in Kingsport, Tennessee. As specified in the Cooperative Agreement, the Partnership developed an Environmental Monitoring Plan (EMP) (August 1996) which describes in detail the environmental monitoring activities to be performed during the operation of the LPMEOH™ Demonstration Unit. The purpose of the EMP is to: 1) document the extent of compliance monitoring activities, i.e., those activities required to meet permit requirements, 2) confirm the specific environmental impacts predicted in the National Environmental Policy Act documentation, and 3) establish an information base for the assessment of the environmental performance of the technology for future commercialization.

The EMP describes three categories of environmental monitoring which are performed as a result of the operation of the LPMEOH™ Demonstration Unit. Details of streams internal to the demonstration unit are available in the Technical Progress Reports for the Project.

4.1 Eastman Reporting of Publicly Available Technical Data

As defined in the Statement of Work for the Demonstration project, Eastman will provide data on three areas of operation of the Chemicals-from-Coal complex (refer to Table 4.1 for a breakdown of the streams to be monitored):

- 1) Gasifier material balance data
- 2) 10C-30 Guard Bed operating data
- 3) Wastewater and alcohols to wastewater treatment system

This technical information provides information from Eastman's existing facilities to provide an overall assessment of the LPMEOH™ technology. A separate Topical Report

(during Year 1 of the operation of the demonstration unit) provides this information, and a summary is available in the Year 1 Annual Environmental Monitoring Report (EMR). Updates, if any, are included in Quarterly EMRs if a significant change occurs.

4.2 Compliance Monitoring

Four areas of compliance monitoring have been identified to satisfy the permit requirements for the demonstration unit (Table 4.2):

- 1) Combined Vapor Flow from Demonstration Unit to Boiler
- 2) Fugitive Emissions
- 3) Particulate Emissions
- 4) Wastewater Treatment System Outlet Stream

Each of these sources is monitored at a frequency mandated by the relevant permit or industrial hygiene practice. The EMRs will include the results of any compliance monitoring generated during the reporting period.

4.3 Supplemental Monitoring

Three areas of supplemental monitoring have been identified in the EMP (Table 4.3):

Summary of Major Material Balance Streams for Demonstration Unit

The major feed streams (CO Gas, H₂ Gas, Balanced Gas) and product flows (Refined Grade Methanol, Crude Grade Methanol, Main Plant Purge) are provided as a summary table of the cumulative stream flows for the reporting period.

Solid/Liquid Discharges

Four other streams can be generated from the demonstration unit:

- 1) Compressor and Pump Lubricants
- 2) Oil Recovered in Oil/Water Separator
- 3) Spent Catalyst
- 4) 29C-40 Guard Bed Adsorbent

Any quantities generated during the reporting period are included in the EMR.

Noise

A noise survey around the 29K-01 Recycle Compressor is planned during the initial start-up of the demonstration unit. The EMR covering activities during the initial operation of the demonstration unit will include the results of this noise survey.

TABLE 4.1
LPMEOH™ DEMONSTRATION UNIT
**PUBLICLY AVAILABLE TECHNICAL DATA FROM EASTMAN
 CHEMICALS-FROM-COAL COMPLEX**

| <u>Environmental Media</u> | <u>General Parameters</u> |
|---|---|
| Coal | Pressure, Temperature, Coal Analysis |
| Oxygen to Gasifier | Pressure, Temperature, %O ₂ |
| Water to Gasifier | Pressure, Temperature |
| Waste Water from Gasifier | Pressure, Temperature, Total Organic Carbon |
| Clean Synthesis Gas from Gasifier | Pressure, Temperature, Flow |
| Sulfur Recovered from Gasifier | Pressure, Temperature, Flow, %S |
| Carbon Dioxide from Gasifier | Pressure, Temperature, Flow, %CO ₂ |
| Slag from Gasifier | Pressure, Temperature, Flow |
| Balanced Gas from 10C-30 Guard Bed | Pressure, Temperature, Flow, Composition |
| Wastewater and Alcohols to Wastewater Treatment System | Flow, Composition, BOD |

TABLE 4.2
LPMEOH™ DEMONSTRATION UNIT
COMPLIANCE MONITORING

| <u>Environmental Media</u> | <u>General Parameters</u> |
|---|---|
| Combined Vapor Flow from Demonstration Unit to Boiler | Composition |
| Fugitive Emissions | Leak Detection and Repair (LDAR) Report, Volatile Organic Carbon (VOC), Background Ambient CO Concentration |
| Particulate Emissions | Threshold Limit Value (TLV) |
| Wastewater Treatment System Outlet Stream | Flow, Total Organic Carbon, pH |

TABLE 4.3
LPMEOH™ DEMONSTRATION UNIT
SUPPLEMENTAL MONITORING

| <u>Environmental Media</u> | <u>General Parameters</u> |
|--|-----------------------------|
| CO Gas to LPMEOH™ Demonstration Unit | Cumulative Flow for Quarter |
| H ₂ Gas to LPMEOH™ Demonstration Unit | Cumulative Flow for Quarter |
| Balanced Gas to LPMEOH™ Demonstration Unit | Cumulative Flow for Quarter |
| Main Vapor Purge from LPMEOH™ Demonstration Unit | Cumulative Flow for Quarter |
| Refined Grade Methanol | Cumulative Flow for Quarter |
| Crude Grade Methanol | Cumulative Flow for Quarter |
| Compressor and Pump Lubricants | Weight or Volume |
| Oil Recovered in Oil/Water Separator | Weight or Volume |
| Spent Catalyst | Weight, Weight% Solids |
| 29C-40 Guard Bed Adsorbent | Weight or Volume |
| Noise Survey for 29K-01 Recycle Compressor | dBa |

5. Project Summary

Synthesis gas was first introduced to the LPMEOH™ Demonstration Unit on 02 April 1997. The nameplate capacity of 80,000 gallons of methanol per day (260 tons-per-day) was achieved on 06 April 1997. Table 5.1 summarizes the onstream time and outages of the LPMEOH™ Demonstration Unit during the reporting period.

6. Updates on Eastman "Chemicals-from Coal" Facility Publicly Available Technical Data

6.1 Gasifier Facility

The report on publicly available technical data from the Eastman "Chemicals-from-Coal" facility, which includes data on the streams associated with the Gasifier facility, will be issued during the first year of operation of the LPMEOH™ Demonstration Unit.

6.2 10C-30 Catalyst Guard Bed

The report on publicly available technical data from the Eastman "Chemicals-from-Coal" facility, which includes data on the streams around and the operation of the 10C-30 Catalyst Guard Bed, will be issued during the first year of operation of the LPMEOH™ Demonstration Unit.

There was no change in the operation of the 10C-30 Catalyst Guard Bed during the reporting period. No new catalyst was added to or removed from the vessel.

6.3 Wastewater and Alcohols to Wastewater Treatment System

The report on publicly available technical data from the Eastman "Chemicals-from-Coal" facility, which includes data on the streams associated with the wastewater and alcohols to the Wastewater Treatment System, will be issued during the first year of operation of the LPMEOH™ Demonstration Unit. This will consist of a comparison of the flow, composition, and BOD load of this stream before and after the addition of the LPMEOH™ Demonstration Unit.

Table 5.1

Summary of LPMEOH™ Demonstration Unit Onstream Time and Outages - April/June 1997

| Operation Start | Operation End | Operating Hours | Shutdown Hours | Reason for Shutdown |
|------------------------|---------------|-----------------|----------------|---|
| 4/2/97 09:00 | 4/2/97 16:15 | 7.3 | 4.8 | Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 4/2/97 21:05 | 4/2/97 21:25 | 0.3 | 23.3 | Liquids to K-01 |
| 4/3/97 20:40 | 4/4/97 11:00 | 14.3 | 24.8 | Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 4/5/97 11:45 | 4/6/97 01:45 | 13.0 | 5.8 | C-03 Outlet Plugged |
| 4/6/97 07:30 | 4/7/97 13:05 | 29.6 | 2.1 | C-03 Outlet Plugged |
| 4/7/97 15:10 | 4/8/97 06:30 | 15.3 | 21.5 | Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 4/9/97 04:00 | 4/9/97 05:30 | 1.5 | 4.0 | ESD on C-02 Level |
| 4/9/97 09:30 | 4/9/97 14:20 | 4.8 | 9.7 | Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 4/10/97 00:00 | 4/11/97 08:25 | 32.4 | 14.8 | Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 4/11/97 23:15 | 4/18/97 18:05 | 162.8 | 0.7 | Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 4/18/97 18:45 | 4/19/97 07:50 | 13.1 | 0.7 | Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 4/19/97 08:30 | 4/23/97 00:20 | 87.8 | 20.7 | Replace TV-101 Trim |
| 4/23/97 21:00 | 4/23/97 21:00 | 0.0 | 12.0 | * Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 4/24/97 09:00 | 5/8/97 23:59 | 351.0 | 950.1 | ** Syngas Unavailable to LPMEOH™ Demonstration Unit |
| 6/17/97 14:05 | 6/30/97 23:59 | 321.9 | | |
| Total Operating Hours | | 1055.2 | | |
| Syngas Available Hours | | 1112.0 | | |
| Plant Availability, % | | 94.9 | | |

* Plant was ready to startup, but Eastman waited 12 hours to give the day crew training
on startup procedures.

** Eastman complex outage.

7. Compliance Monitoring

7.1 Combined Vapor Flow from Demonstration Unit to Boiler

A sample of the header gas from the LPMEOH™ Demonstration Unit must be analyzed as part of the Boiler and Industrial Furnace regulations within RCRA. Sampling is currently required every three years. The next sample will be taken in February of 2000.

No activity occurred during the reporting period.

7.2 Fugitive Emissions

7.2.1 Leak Detection and Repair (LDAR)

No activity occurred during the reporting period. The next report on Leak Detection and Repair is anticipated for December of 1997.

7.2.2 Ambient Carbon Monoxide Background Concentration

This one-time study will record the concentration of CO that is encountered by a LPMEOH™ operations person during the course of a normal day of plant operations.

No activity occurred during the reporting period. The ambient CO background concentration study is scheduled to be performed during the first quarter of 1998.

7.3 Particulate Emissions

This one-time study will record the exposure level to particulate emissions that is encountered by a LPMEOH™ operations person during the catalyst charging process.

The report on this study is included in Appendix B. The results show that the concentrations of aluminum and zinc were below the Threshold Limit Value (TLV) of 10 mg/m³, but that the copper concentrations may exceed the TLV. However, it should be noted that operators use respiratory protection during the catalyst loading operation. Some engineering modifications are planned to reduce the dust concentration.

7.4 Wastewater Treatment System Outlet Stream

The reports on the outfall from the Wastewater Treatment System (Discharge Number 002) for the reporting period is attached in Appendix C. There were no permit excursions.

A process stream within the existing Eastman facility which is impacted by the operation of the LPMEOH™ Demonstration Unit contains the byproduct alcohols and water which are generated in parallel with the production of methanol. This stream is sent to the Eastman Wastewater Treatment System. The annual EMR will contain a comparison of the flow,

composition, and BOD load of this stream before and after the addition of the LPMEOH™ Demonstration Unit.

8. Supplemental Monitoring

8.1 Total Synthesis Gas Use and Methanol Production

Table 8.1 contains the summary of the major process flows to and from the LPMEOH™ Demonstration Unit for the reporting period. Almost 3,000,000 gallons of methanol (Refined and Crude Grades) were produced during the reporting period.

8.2 Oil/Water Separator

Since the startup of the LPMEOH™ Demonstration Unit, about 16,000 pounds of oil have been removed from the Oil/Water Separator. This material is presently stored in drums awaiting final disposition by incineration for energy recovery.

8.3 Compressor and Pump Lubricants

No material was generated during the reporting period.

8.4 Spent Catalyst Slurry

Approximately 300 pounds of methanol synthesis catalyst were removed from the LPMEOH™ reactor during the outage between 08 May and 17 June 1997. This material is presently stored onsite and will be included as part of the first large shipment of spent catalyst to the off-site catalyst reclaimer.

8.5 29C-40 Catalyst Guard Bed Spent Adsorbent

No material was generated during the reporting period.

8.6 Noise

A noise survey of the entire LPMEOH™ Demonstration Unit was performed during the reporting period. This was performed to determine if operators working in the plant were exposed to sound levels at which annual audiometric testing would be required. The results of this survey are included in Appendix D. Noise dosimetry results found operator exposures to be less than the 50% of the threshold dose for placement of operators working in the LPMEOH™ Demonstration Unit on a list for required annual audiometric testing. No additional testing of operators is required.

The noise survey around the 29K-01 Recycle Compressor is a one-time test and is scheduled to be completed during the third quarter of 1997.

Table 8-1
Synthesis Gas Use and Methanol Production - April/June 1997
LPMEOH™ Demonstration Unit

| | April 1997 | May 1997 | June 1997 | Total |
|--------------------------|------------|-----------|-----------|-----------|
| Consumption, KSCF | | | | |
| Balanced Gas | 449,783.0 | 123,586.5 | 211,488.0 | 784,857.5 |
| CO Gas | 0.0 | 1,496.4 | 0.0 | 1,496.4 |
| H ₂ Gas | 0.0 | 0.0 | 0.0 | 0.0 |
| Production, Tons | | | | |
| Crude Methanol | 1,530.1 | 367.2 | 597.0 | 2,494.3 |
| Refined Methanol | 3,940.5 | 1,077.0 | 2,061.5 | 7,079.0 |
| Total Purge Gas, KSCF | 33,400.0 | 19,938.0 | 28,495.6 | 81,833.6 |

9. Compliance

9.1 Compliance with Permit Limits

There were no excursions outside permit limits associated with the operation of the LPMEOH™ Demonstration Unit.

10. Problems and Recommendations

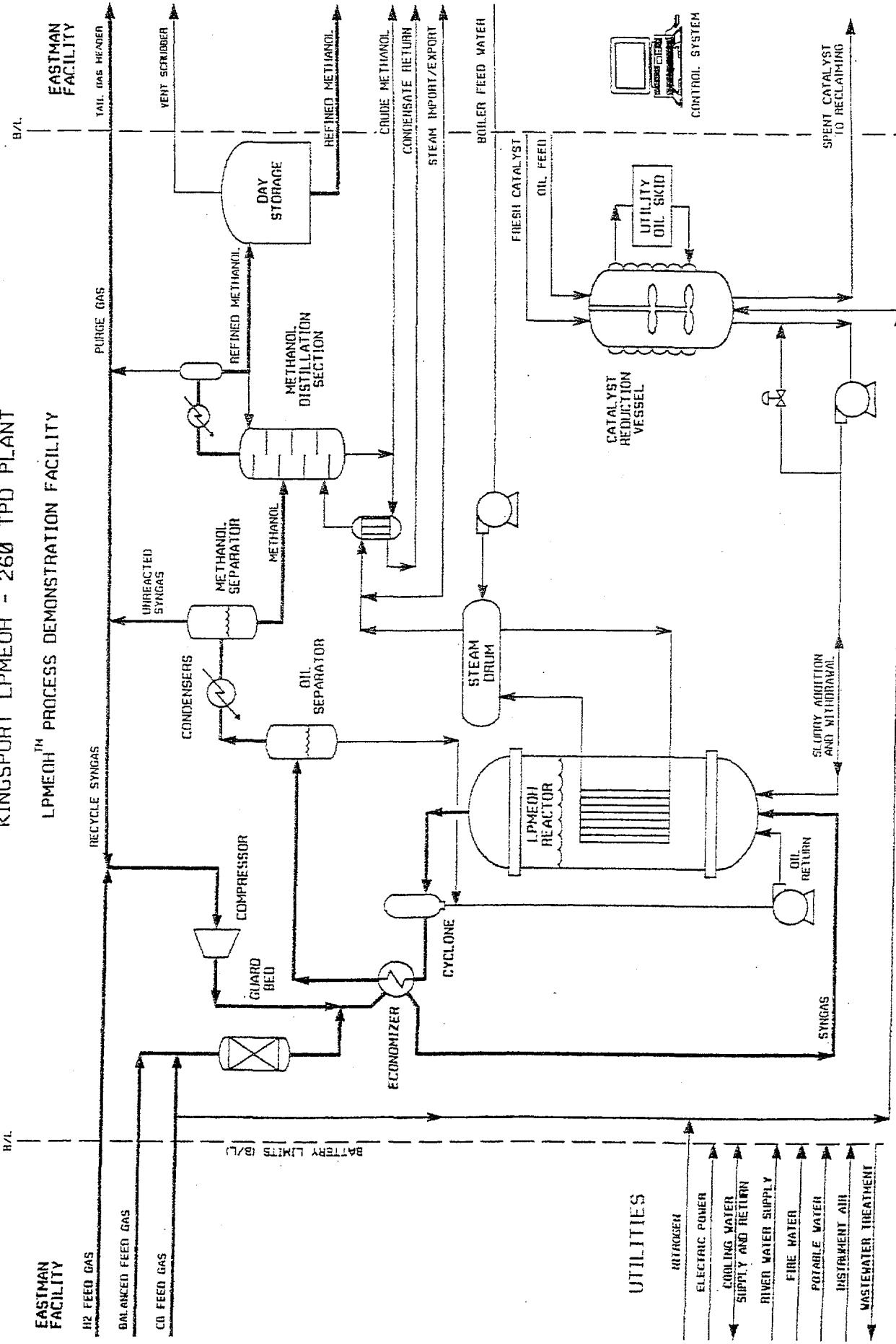
There have been no significant problems arising in the environmental area.

APPENDICES

APPENDIX A - SIMPLIFIED PROCESS FLOW DIAGRAM

SIMPLIFIED PROCESS DIAGRAM
KINGSPORT LPMEOH - 260 TPD PLANT

LPMEOH™ PROCESS DEMONSTRATION FACILITY



APPENDIX B - DUST EXPOSURE SURVEY DURING CATALYST LOADING

Title: Operator Exposures to Aluminum, Copper & Zinc - Liquid Phase Methanol Plant, B-486

Abstract: Copper dust concentrations may exceed the ACGIH Threshold Limit Value (TLV) of 1 mg/m³ during the catalyst charging operation. Respiratory protection is currently used to ensure exposure is controlled to an acceptable level.

Recommendation: 1) Implement planned engineering modifications to reduce dust concentrations during the charging of catalyst.

On July 22, 1997, breathing zone (BZ) samples were collected during the charging of copper catalyst in B-486 as a follow-up to earlier data collected in March. In March, sampling data indicated that airborne copper concentrations may exceed the TLV. In addition, samples for the aluminum and zinc components of the catalyst were collected. Normally, six drums (1050 kg) of catalyst are charged to a hopper using a drum hoist. Catalyst make-up is done about once every 2-3 weeks.

The following 8-hr time-weighted copper concentrations were found:

| Copper | 3/16 | 3/26 | 7/22 |
|----------------------------|-------------|-----------|-----------|
| Mean (mg/m ³) | >1.0* | 0.7 | 0.2 |
| Range (mg/m ³) | 0.1 - >2.0* | 0.6 - 0.7 | 0.1 - 0.4 |

Note: asterisk denotes concentrations above 1 mg/m³ TLV

Currently, dust generation is minimized by means of a "plastic sock" which is attached to the drums prior to charging. This interim measure appears to be successful as indicated by the above copper concentrations. The planned engineering modifications include a funnel system on the drum hoist.

The (BZ) samples collected for aluminum and zinc found all concentrations to be substantially less than the ACGIH TLV of 10 mg/m³ established for these materials. Please share the results of this report with all operators involved in the catalyst charging process. Also, please contact Industrial Hygiene to reevaluate dust concentrations after completion of the equipment modifications.

Steve L. Drushel
Steve L. Drushel
JHF

**APPENDIX C - NPDES REPORTS FOR WASTEWATER TREATMENT SYSTEM
OUTLET STREAM**

PERMITTEE NAME/ADDRESS:

TN EASTMAN DIVISION
DIVISION OF EASTMAN CHEMICAL CO.
P.O BOX 1983
KINGSPORT, TN 37682-5383

NATIONAL POLLUTANT DISCHARGE ELIMINATION SYSTEM (NPDES)

FORM APPROVED
OMB No.2040-0004

TN0002640
PERMIT NUMBER

(SUBR 05)

F - FINAL

MAJOR

EFFLUENT

NO DISCHARGE

... NO DISCHARGE

INDUSTRIAL PROCESS WASTEWATER
NOTE: Read instructions before completing this form.

DISCHARGE MONITORING REPORT (MARY)

002 G

DISCHARGE NUMBER

MONITORING PERIOD

97 - 04 - 01 TO 97 - 04 - 30

NOTE: Read instructions before completing this form.

FROM NO. EX (64-59)
TO NO. EX (64-68)

Frequency of analysis

Continuous

(64-69)

Sample Type (69-70)

N/A

(3 Card Only)
(45-55)

Quantity or (54-61)

Concentration (46-53)

(54-61)

NO. EX (64-59)

NO. EX (64-68)

Frequency of analysis

Continuous

(64-69)

Sample Type (69-70)

N/A

MEASUREMENT

Average

Maximum

Unit

Minimum

Average

Maximum

Unit

Frequency of analysis

Continuous

(64-69)

Sample Type (69-70)

N/A

SOLIDS, TOTAL

SUSPENDED

EFFLUENT GROSS VALUE

PERMIT REQUIREMENT

MEASUREMENT

AVERAGE

DAILY MAX

LBS/DAY

Frequency of analysis

Continuous

(64-69)

Sample Type (69-70)

N/A

NITROGEN, AMMONIA
TOTAL (AS N)

EFFLUENT NET VALUE

PERMIT REQUIREMENT

MEASUREMENT

AVERAGE

DAILY MAX

LBS/DAY

Frequency of analysis

Continuous

(64-69)

Sample Type (69-70)

N/A

CHROMIUM, TOTAL (AS CR)

EFFLUENT NET VALUE

PERMIT REQUIREMENT

MEASUREMENT

AVERAGE

DAILY MAX

LBS/DAY

Frequency of analysis

Continuous

(64-69)

Sample Type (69-70)

N/A

COPPER, TOTAL (AS CU)

EFFLUENT NET VALUE

PERMIT REQUIREMENT

MEASUREMENT

AVERAGE

DAILY MAX

LBS/DAY

Frequency of analysis

Continuous

(64-69)

Sample Type (69-70)

N/A

LEAD, TOTAL (AS PB)

EFFLUENT NET VALUE

PERMIT REQUIREMENT

MEASUREMENT

AVERAGE

DAILY MAX

LBS/DAY

Frequency of analysis

Continuous

(64-69)

Sample Type (69-70)

N/A

COMMENT AND EXPLANATION OF ANY VIOLATIONS

In addition to taking reasonable steps to prevent instances of noncompliance through the implementation of SPCC and SPCG-type plans, employee training, etc. when a potentially significant instance occurs, we notify the Division and provide information concerning the steps taken or planned to reduce, eliminate, and prevent recurrence of the instance.

(REPLACES EPA FORM T-40 WHICH MAY NOT BE USED.)

EPA FORM 3120-1 (REV. 8-88) Previous editions may be used.

TYPE OR PRINTED

John F. Holliman

H. H. Holliman, President

Tennessee Eastman Division

SIGNATURE OF PRINCIPAL EXECUTIVE OFFICER OR AUTHORIZED AGENT

John F. Holliman

John F. Holliman

PERMITTEE NAME/ADDRESS:
TN EASTMAN DIVISION
DIVISION OF EASTMAN CHEMICAL CO.
P.O. BOX 1993
KINGSPORT, TN 37662-5393

NATIONAL POLLUTANT DISCHARGE ELIMINATION SYSTEM (NPDES)

FORM APPROVED
OMB No. 2040-0004TN0002640
PERMIT NUMBER

DISCHARGE MONITORING REPORT (DMR)

(SUBR 06)

F - FINAL

PROCESSED W/W QUARTERLY REPORT

EFFLUENT

Facility: TN EASTMAN - KINGSPORT

Location: SULLIVAN COUNTY TN 37662-5393

... NO DISCHARGE L...
NOTE: Read Instructions before completing this form.

| MONITORING PERIOD | |
|-------------------|-------------|
| FROM | TO |
| 97 - 04 - 01 | 97 - 06 -30 |

| PARAMETER (#2-3) | Quantity or (#4-5) | Loading (#2-5) | (4 Card Only) (#6-9) | | | Concentration (#4-6) | NO. EX (#2-4) | Frequency of analysis (#4-6) | Simple Type (#9-70) |
|---|-----------------------|---|---------------------------|------------------|----------------------------------|-------------------------|------------------|------------------------------------|---|
| | | | Average | Maximum | Unit | | | | |
| NITROBENZENE | SAMPLE | MEASUREMENT | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| 34447 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONDAY | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| PIENANTHRENE | SAMPLE | MEASUREMENT | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| 34461 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONDAY | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| PYRENE | SAMPLE | MEASUREMENT | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| 34469 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONDAY | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| TETRACHLOROETHYLENE | SAMPLE | MEASUREMENT | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| 34476 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONDAY | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| 1,1 - DICHLOROETHANE | SAMPLE | MEASUREMENT | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| 34496 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONDAY | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| 1,1,1 - TRICHLOROETHANE | SAMPLE | MEASUREMENT | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| 34501 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONDAY | BDL | (26) | LBS/DAY | 0.000000 | BDL | (19) 0 | Grab |
| NAME/TITLE PRINCIPAL EXECUTIVE OFFICER H. H. Holliman, President | TYPED OR PRINTED | SIGNATURE OF PRINCIPAL EXECUTIVE <i>H. H. Holliman</i> | TELEPHONE 615 224 7268 | DATE 07-07-97 | AREA CODE NUMBER 423 229-2000 | YEAR 97 | MONTH 07 | DAY 11 | (REPLACES EPA FORM T-40 WHICH MAY NOT BE USED.) |

COMMENT AND EXPLANATION OF ANY VIOLATIONS
in addition to taking reasonable steps to prevent instances of noncompliance through the implementation of SPCC and SPCC-type plans, employee training, etc. When a potentially significant instance occurs, we notify the Division and provide information concerning the steps taken or planned to reduce, eliminate, and prevent recurrence of the instance.

EPA FORM 3320-1 (REV. 9-88) Previous editions may be used.

(Reference all attachments here)

Identify areas of noncompliance that have been successfully handled and all parties within the organization identified herein and dated only if required by those individuals who ultimately responsible for obtaining this information. I assure that this is as soon as can be reasonably practical. I AM ASKING THAT THIS INFORMATION BE KEPT CONFIDENTIAL AND NOT MADE PUBLIC. THE POSSIBILITY OF PUBLISHING THIS INFORMATION IN THE NEWS MEDIA AND/OR USE IN THE COURTS MAY PREVENT ME FROM DOING THIS FOR A PERIOD OF ONE YEAR AND ONLY WITH THE APPROVAL OF MY ATTORNEY AND MY ATTORNEY'S FIRM.

(REPLACES EPA FORM T-40 WHICH MAY NOT BE USED.)

TN EASTMAN DIVISION
DIVISION OF EASTMAN CHEMICAL CO.
P.O. BOX 1993
KINGSPORT, TN 37662-5393

NATIONAL POLLUTANT DISCHARGE ELIMINATION SYSTEM (NPDES)
DISCHARGE MONITORING REPORT (DMR)
TN0002640
PERMIT NUMBER

FORM APPROVED
OMB No. 7040-0004
(SUBR 08)
F - FINAL
PROCESSED WWW QUARTERLY REPORT
EFFLUENT

Facility: SULLIVAN COUNTY TN 37662-5393

MONITORING PERIOD
FROM 97-04-01 TO 97-06-30
NO DISCHARGE L...

NOTE: Read instructions before completing this form.

| PARAMETER (#33) | (3 Card Only) (46-50) | | Quantity or (4 Card Only) (46-61) | | Loading (48-49) | | Quality or (46-53) | | Concentration (44-47) | | NO. EX (61-63) | Frequency of analysis (64-66) | Sample Type (69-70) |
|---|---|-------------|---|-----------|--------------------|-----------|-----------------------|-----------|--------------------------|-----------|----------------------|-------------------------------------|---------------------------|
| | Average | Maximum | Unit | Minimum | Average | Maximum | BDL | BDL | BDL | BDL | | | |
| 2,4 - DINITROPHENOL | SAMPLE | MEASUREMENT | BDL | (26) | BDL | BDL | BDL | BDL | BDL | BDL | (19) | 0 | 2/Quarter |
| 34816 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONAVAN | LBS/DAY | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MGL | 0 | QUARTERLY |
| 2,6 - DINITROTOLUENE | SAMPLE | MEASUREMENT | BDL | (26) | BDL | BDL | BDL | BDL | BDL | BDL | (19) | 0 | QUARTERLY |
| 34676 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONAVAN | LBS/DAY | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MGL | 0 | QUARTERLY |
| 4 - NITROPHENOL | SAMPLE | MEASUREMENT | BDL | (26) | BDL | BDL | BDL | BDL | BDL | BDL | (19) | 0 | 2/Quarter |
| 34646 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONAVAN | LBS/DAY | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MGL | 0 | QUARTERLY |
| 4,6 - DINITRO - O - CRESOL | SAMPLE | MEASUREMENT | BDL | (26) | BDL | BDL | BDL | BDL | BDL | BDL | (19) | 0 | 2/Quarter |
| 34697 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONAVAN | LBS/DAY | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MGL | 0 | QUARTERLY |
| PHENOL, SINGLE COMPOUND | SAMPLE | MEASUREMENT | BDL | (26) | BDL | BDL | BDL | BDL | BDL | BDL | (19) | 0 | 2/Quarter |
| 34694 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONAVAN | LBS/DAY | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MGL | 0 | QUARTERLY |
| NAPHTHALENE | SAMPLE | MEASUREMENT | BDL | (26) | BDL | BDL | BDL | BDL | BDL | BDL | (19) | 0 | 2/Quarter |
| 34696 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONAVAN | LBS/DAY | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MGL | 0 | QUARTERLY |
| ETHYL BENZENE | SAMPLE | MEASUREMENT | BDL | (26) | BDL | BDL | BDL | BDL | BDL | BDL | (10) | 0 | 2/Quarter |
| 37371 2 0 0 EFFLUENT NET VALUE | PERMIT REQUIREMENT | MONAVAN | LBS/DAY | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MONAVAN | MGL | 0 | QUARTERLY |
| NAME/TITLE PRINCIPAL EXECUTIVE OFFICER | H. H. Holloman, President | TELEPHONE | 224 7260 | TELEPHONE | 224 7260 | TELEPHONE | 224 7260 | TELEPHONE | 224 7260 | TELEPHONE | TELEPHONE | DATE | TELEPHONE |
| COMMENT AND EXPLANATION OF ANY VIOLATIONS | I CERTIFY UNDER PENALTY OF PERJURY THAT THE INFORMATION PROVIDED HEREIN WAS MADE ORIGINALLY IN MY OWN KNOWLEDGE AND THAT IT IS TRUE AND CORRECT TO THE BEST OF MY KNOWLEDGE AND BELIEF. I AM AWARE THAT THIS INFORMATION IS FOR RECORDS AND INFORMATION PURPOSES ONLY. ACCORDING TO THE RECORDS OF THE STATE OF TENNESSEE, THE PERSON SIGNING THIS FORM IS AN EMPLOYEE OF THE STATE OF TENNESSEE AND IS SUBJECT TO THE PENALTIES PROVIDED FOR IN TENNESSEE CODE OF CRIMES AND CRIMINAL PROCEDURE, SECTION 40-14-101 AND 40-14-102. I HEREBY CERTIFY THAT THIS INFORMATION IS FOR RECORDS AND INFORMATION PURPOSES ONLY. ACCORDING TO THE RECORDS OF THE STATE OF TENNESSEE, THE PERSON SIGNING THIS FORM IS AN EMPLOYEE OF THE STATE OF TENNESSEE AND IS SUBJECT TO THE PENALTIES PROVIDED FOR IN TENNESSEE CODE OF CRIMES AND CRIMINAL PROCEDURE, SECTION 40-14-101 AND 40-14-102. | | | | | | | | | | | | |
| TYPED OR PRINTED | John H. Holloman <i>John H. Holloman</i> Signature of Principal Executive Officer or Authorized Agent | | | | | | | | | | | | |
| NAME | (REPLACES EPA FORM T-40 WHICH MAY NOT BE USED.) | | | | | | | | | | | | |
| AREA CODE NUMBER | (423) 229-2000 97 - 07 - 11 | | | | | | | | | | | | |
| YEAR MO DAY | YEAR MO DAY | | | | | | | | | | | | |

In addition to taking reasonable steps to prevent instances of noncompliance through the implementation of SPCC and SPCC-type plans, employee training, etc. when a potentially significant instance occurs, we notify the Division and provide information concerning the steps taken or planned to reduce, eliminate, and prevent recurrence of the instance.

EPA FORM 3320-1 (REV. 9-98) Previous editions may be used.

Reference all attachments here.

PAGE 7 OF 8
(REPLACES EPA FORM T-40 WHICH MAY NOT BE USED.)

APPENDIX D - PLANT-WIDE NOISE DOSIMETRY MEASUREMENTS

Title: Noise Dosimetry Measurements - Liquid Phase Methanol, Plant 29

Abstract: Noise dosimetry results found operator exposures associated with this job code to be less than the 50% threshold dose for placement on the list for annual audiograms.

Recommendation: Inform operators working in Plant 29 of the results of this report.

On April 26-27 and May 5, 1997, measurements were taken to initially determine operator exposure to noise in the newly-constructed Liquid Phase Methanol Plant. This information is used to determine the persons to receive annual audiometric testing by job code or description.

The five measurements indicated noise doses ranging from 16.2% - 39.7% with a mean value of 26.3%. A 50% dose (equivalent to 82 dBA as averaged over 12 hours) is the threshold criteria. Based on this information, the operators working in Plant 29 will not be placed on the annual audiometric testing list as a result of charging time to cost center 4113.

Steve L. Drushel
Steve L. Drushel

JHJ
6-9-97